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# **Cationic Adsorption-Induced Microlevelling Effect: A Pathway to Dendrite-Free Zinc Anodes**

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# HIGHLIGHTS

- A microlevelling agent containing Gd<sup>3+</sup> ions significantly enhances the reversibility and stability of zinc anodes.
- Gd<sup>3+</sup> ions are preferentially adsorbed onto zinc surface, shielding zinc deposition at protrusions.
- Adsorbed Gd<sup>3+</sup> ions establish a water-poor electric double layer, suppressing side reactions at the interface.

**ABSTRACT** Dendrite growth represents one of the most significant challenges that impede the development of aqueous zinc-ion batteries. Herein,  $Gd^{3+}$  ions are introduced into conventional electrolytes as a microlevelling agent to achieve dendrite-free zinc electrodeposition. Simulation and experimental results demonstrate that these  $Gd^{3+}$  ions are preferentially adsorbed onto the zinc surface, which enables dendritefree zinc anodes by activating the microlevelling effect during electrodeposition. In addition, the  $Gd^{3+}$  additives effectively inhibit side reactions and facilitate the desolvation of  $[Zn(H_2O)_6]^{2+}$ , leading to highly reversible zinc plating/strip-



ping. Due to these improvements, the zinc anode demonstrates a significantly prolonged cycle life of 2100 h and achieves an exceptional average Coulombic efficiency of 99.72% over 1400 cycles. More importantly, the  $Zn//NH_4V_4O_{10}$  full cell shows a high capacity retention rate of 85.6% after 1000 cycles. This work not only broadens the application of metallic cations in battery electrolytes but also provides fundamental insights into their working mechanisms.

KEYWORDS Aqueous zinc-ion batteries; Zinc anodes; Rare-earth cations; Microlevelling; Zinc dendrites

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# **1** Introduction

Aqueous zinc-ion batteries (AZIBs) are widely regarded as promising candidates for large-scale energy storage systems owing to their superior advantages in cost, safety, and resource availability [1-3]. However, their practical employment is hindered by rapid dendrite evolution caused by uneven zinc deposition during charge/discharge [4-6]. At the microscopic scale, zinc anodes typically exhibit a rough and irregular surface morphology. This morphological irregularity results in a tipping effect where charges accumulate at protrusions on the anode surface, creating localized electric field and concentrated  $Zn^{2+}$  fluxes [7, 8]. During zinc deposition, these concentrated  $Zn^{2+}$  ions preferentially deposit on the protrusions, leading to the formation of dendrites. The growth of dendrites further exacerbates the tipping effect, resulting in uncontrollable zinc dendrite growth that can ultimately induce short circuits within the battery [9]. Additionally, water molecules tend to be adsorbed on the negatively charged zinc surface, forming a water-rich electric double layer (EDL) [10]. The interfacial water molecules, particularly those located near the dendrites, can easily trigger a series of side reactions, including zinc corrosion, hydrogen evolution reaction (HER), and by-product formation [11, 12]. Therefore, inhibiting zinc dendrite growth is essential for improving the stability and overall performance of AZIBs.

To address the issue of zinc dendrites, many strategies have been proposed, primarily focusing on anode modification [13–18], separator functionalization [19], and electrolyte engineering [20–25]. Among these strategies, incorporating functional additives into electrolytes has emerged as one of the most promising approaches. For instance, organic additives such as dimethyl sulfoxide [21] and dimethylformamide [22] have been shown to effectively inhibit zinc dendrite growth by modulating the Zn<sup>2+</sup> solvation structures. However, the use of flammable organic molecules compromises battery safety and increases battery polarization. Moreover, the continuous decomposition of organic additives can lead to thickening of the interphase layer, ultimately resulting in unsatisfactory battery performance [26]. In contrast, inorganic salts containing metallic cations (e.g., Li<sup>+</sup> [20], Mg<sup>2+</sup> [23], Ce<sup>3+</sup> [27], La<sup>3+</sup> [28], Y<sup>3+</sup> [29]) are highly effective and durable in regulating zinc deposition behavior. Compared to monovalent and divalent cations, trivalent cations demonstrate superior effectiveness in inhibiting dendrite growth due to their stronger electrostatic interactions with the charged zinc surface and  $Zn^{2+}$ ions. Additionally, metallic cations have been widely used as electrolyte additives in conventional zinc electroplating technologies to improve coating homogeneity and corrosion resistance [30]. Given the critical role of metallic cations in regulating the zinc–electrolyte interface, further exploit their potential and understand their working mechanisms in AZIBs is of significant importance.

Herein, we introduce the heavy rear-earth (RE) cation Gd<sup>3+</sup> into a conventional 3 M ZnSO<sub>4</sub> (ZSO) electrolyte as a microlevelling agent to achieve dendrite-free zinc deposition. As schematically illustrated in Fig. 1,  $Gd^{3+}$  ions are preferentially adsorbed on to the zinc surface, thereby enhancing anode stability by activating the microlevelling effect. This mechanism stands in stark contrast to the rapid dendrite growth caused by the tipping effect in conventional ZSO electrolyte. In additional, the electrostatically adsorbed  $Gd^{3+}$  ions synergistically shield the protruding zinc surface from water molecules, suppressing detrimental side reactions such as HER and by-product formation. Consequently, highly reversible and dendrite-free zinc anodes could be achieved with the Gd<sup>3+</sup> microlevelling agent. Leveraging these benefits of the Gd<sup>3+</sup>-containing electrolyte, the cycle life of the Zn//Zn symmetric cell significantly prolongs to over 2100 h at 1 mA cm<sup>-2</sup> and 1 mAh cm<sup>-2</sup>. Furthermore, the Zn//Cu symmetric cell exhibits an exceptional average Coulombic efficiency (CE) of 99.72% over 1400 cycles. The Zn//NH<sub>4</sub>V<sub>4</sub>O<sub>10</sub> full cell also shows a high capacity retention rate of 85.6% after 1000 cycles at 5 A  $g^{-1}$ . This work provides fundamental insights into the utilization of metallic cations for developing highly efficient and reliable AZIBs.

## **2** Experimental

#### 2.1 Preparation of Electrolytes

The ZSO electrolyte was prepared by dissolving 215.67 g of  $ZnSO_4$ ·7H<sub>2</sub>O in 250 mL of deionized (DI) water. Electrolytes with Gd<sup>3+</sup> concentrations of 0.01, 0.02, 0.05, and 0.08 M were obtained by adding specific amounts of Gd<sub>2</sub>(SO<sub>4</sub>)<sub>3</sub>·8H<sub>2</sub>O powder to 30 mL of ZSO solution.



**Fig. 1** Schematic illustrations of the zinc–electrolyte interface in different electrolytes. **a** Solvated  $Zn^{2+}$  ions adsorb on protrusions due to the concentration of electric field, resulting in rampant dendrite growth in the ZSO electrolyte. Meanwhile, the water-rich EDL at the interface leads to severe HER upon zinc deposition. **b** Adsorbed  $Gd^{3+}$  ions activate the microlevelling effect by forming an electrostatic shielding layer at the interface and repels water molecules from the EDL, enabling smooth zinc deposition and suppressing HER in the ZSO/Gd<sup>3+</sup> electrolyte. The gray dashed line represents the virtual profiles of the electric field

#### 2.2 Cell Assembling

The zinc foils with a thickness of 50 µm and a diameter of 15 mm were used as anodes. A glass fiber membrane (Whatman, GF/D) was employed as the separator.  $NH_4V_4O_{10}$ (NVO) powder was synthesized utilizing a hydrothermal method. Specifically, 2.106 g of NH<sub>4</sub>VO<sub>3</sub> was dissolved in 90 mL of DI water under continuous stirring at 80 °C. Subsequently, 3.4038 g of  $H_2C_2O_4 \cdot 2H_2O$  was gradually added to the mixture and kept stirring until the color changed to black green. The resulting solution was divided into three parts, and each part was kept at 140 °C for 48 h in a 50 mL polytetrafluoroethylene autoclave. After the hydrothermal process, the precipitated solids were collected and thoroughly washed with DI water. Finally, the product was dried at 60 °C for 12 h, yielding the desired NVO powder. The NVO, carbon black (Super P), and polyvinylidene fluoride were mixed in a mass ratio of 7:2:1 and dry-milled for 20 min. Subsequently,

N-methyl-2-pyrrolidone was added to the solids and further milled for 10 min. The resulting slurry was uniformly coated onto stainless-steel meshes with a diameter of 12 mm. The coated meshes were placed in a vacuum oven kept at 80 °C for 12 h to obtain the NVO electrodes. The loading of NVO was maintained within the range of 0.9–1.4 mg cm<sup>-2</sup>.

#### 2.3 Electrochemical Measurements

Cyclic voltammetry (CV) measurements for Zn//Cu half cells were conducted on an electrochemical workstation (CHI660E) within the potential range of -0.2 to 1.0 V at 1 mV s<sup>-1</sup>. CV measurements for full cells were conducted at 0.1 mV s<sup>-1</sup> within the voltage range of 0.4–1.4 V. Electrochemical impedance spectroscopy (EIS) curves of symmetric and full cells were obtained within the frequency range of 0.01–10<sup>5</sup> Hz. Chronoamperometry (CA), Tafel, and linear sweep voltammetry (LSV) tests were conducted on the CHI660E electrochemical workstation. Particularly, CA curves were obtained with an overpotential of -150 mV. Tafel tests were conducted within the voltage range of -0.3 to 0.3 V at 10 mV s<sup>-1</sup>. LSV curves were recorded within the voltage range of -0.8 to 0.8 V at a scan rate of 5 mV s<sup>-1</sup>. Constant current charge–discharge and rate tests were conducted on a LAND multi-channel battery testing system (CT2001A).

#### 2.4 Characterizations

Structural characterization of the samples was conducted using an X-ray diffractometer (XRD, Rigaku Mini Flex 600, Cu K $\alpha$  radiation,  $\lambda = 1.5418$  Å) with a detection angle range of 5° < 2 $\theta$  < 80° and a scanning speed of 10° min<sup>-1</sup>. The surface morphology of the zinc anodes was obtained using a scanning electron microscope (SEM, Nova Nano SEM230). The surface roughness of the zinc anodes was measured by a 3D confocal laser scanning microscope (3D-CLSM, KEY-ENCE VK-X1000). An in situ optical microscope (CEWEI LW750LJT) was used to visualize the interface evolution during zinc plating. An energy-dispersive X-ray spectroscopy analyzer (EDS, One Max 50) was employed to characterize the elemental distributions for zinc foils after immersion tests.

#### 2.5 DFT Calculations

All the periodic density functional theory (DFT) calculations were performed on Vienna Ab-initio Simulation Package (VASP). The generalized gradient approximation (GGA) implemented by Perdew–Burke–Ernzerhof (PBE) functional was adopted to describe the exchange–correlation interactions [31]. The valence electronic states were described by expanding plane wave basis set with a kinetic cutoff energy of 400 eV. The (3×3) cells were constructed to model the zinc (002) surface with a vacuum thickness of 15 Å. The adsorption energies ( $E_{ads}$ ) were calculated by:

$$E_{\rm ads} = E_{\rm (slab+Zn)} - E_{\rm slab} - E_{\rm Zn} \tag{1}$$

where  $E_{(\text{slab+Zn})}$  and  $E_{\text{slab}}$  are the total energy of the model surfaces with and without adsorbed Zn<sup>2+</sup> ions, respectively;  $E_{\text{Zn}}$  represents the total energy of an isolated Zn<sup>2+</sup> ion in the gas phase. Calculations of binding energies were performed using the Gaussian09 program [32]. The PBE1PBE/SDD theoretical model was adopted for  $Gd^{3+}$  and  $Zn^{2+}$  ions, and the PBE1PBE/6-31G\* theoretical model was adopted for other atoms [33]. The implicit solvation model, namely the solvation model density (SMD), was used to describe the solvation effect, and all calculations were carried out with atom pairwise dispersion correction (DFT-D3). The binding energy ( $E_b$ ) was calculated by:

$$E_b = E(AB) - E(A) - E(B)$$
<sup>(2)</sup>

where E represents the electronic energy of the component. The visualization of molecular structure was performed using visual molecular dynamics (VMD) [34] and Multiwfn [35].

# **3** Results and Discussion

To determine the optimal electrolyte composition, different Gd<sup>3+</sup> concentrations (0.01, 0.02, 0.05, and 0.08 M) were added to the ZSO electrolyte. Figure S1 presents the Raman spectra of these electrolytes, and two characteristic peaks corresponding to the O-H and SO<sub>4</sub><sup>2-</sup> vibrations were observed. Notably, as the Gd<sup>3+</sup> concentration increases, the intensity of the O-H vibration peak decreases (Fig. 2a), which suggests that the hydrogen bonds (HBs) among water molecules are disrupted by  $Gd^{3+}$  ions [36, 37]. Furthermore, the vibration peak is deconvoluted into three main regions representing strong, weak, and non-HBs (Fig. 2b). The ratio of strong HBs increases with higher Gd<sup>3+</sup> concentrations (Fig. 2c), implying reduced water reactivity [38]. Figure S2 demonstrates the cycling stability of Zn//Zn symmetric cells. As the concentration of  $Gd^{3+}$  ions increases, the Zn//Zn symmetric cells demonstrate enhanced cycling stability. The optimal performance is achieved at a Gd<sup>3+</sup> concentration of 0.05 M, which provides the best balance between enhanced stability and efficient zinc plating/stripping. Further increasing the Gd<sup>3+</sup> concentration to 0.08 M results in rapid failure of the symmetric cell after approximately 300 h. This can be attributed to significantly increased overpotentials resulting from the hindrance of zinc plating/stripping when excessive  $Gd^{3+}$  ions exist in the electrolyte. Based on these findings, the ZSO electrolyte with 0.05 M Gd3+ ions, denoted as ZSO/ Gd<sup>3+</sup> electrolyte, is selected for further investigation.

DFT calculations were performed to elucidate the working mechanisms of  $Gd^{3+}$  ions. As shown in Fig. 2d, the adsorption energy of  $Gd^{3+}$  ions on the zinc (002) surface reaches -2.79 eV, which is significantly lower than the values



**Fig. 2** Characterizations of the electrolytes. **a** Raman spectra of the ZSO and ZSO/Gd<sup>3+</sup> electrolytes with different Gd<sup>3+</sup> concentrations. **b** Deconvolution of HBs and **c** corresponding ratios of different HB types in the electrolytes. **d** Absorption energies of Gd<sup>3+</sup>, Zn<sup>2+</sup>, and H<sub>2</sub>O on the zinc (002) surface. **e** Binding energies of Gd<sup>3+</sup> and Zn<sup>2+</sup> to H<sub>2</sub>O. **f** Calculated solvation structures of Gd<sup>3+</sup> ions with H<sub>2</sub>O

for H<sub>2</sub>O molecules (-0.14 eV) and  $Zn^{2+}$  ions (-0.32 eV). This suggests that Gd<sup>3+</sup> ions can be preferentially adsorbed on the zinc surface, playing a crucial role in activating the microlevelling effect during zinc deposition. Due to their preferential adsorption, Gd<sup>3+</sup> ions will be attracted to the protrusions on the zinc surface and remain effective at their adsorption sites, causing Zn<sup>2+</sup> ions to be repelled and deposited at nearby locations with relatively low heights. Consequently, smooth zinc deposition could be achieved in the ZSO/Gd<sup>3+</sup> electrolyte. Meanwhile, solvated Zn<sup>2+</sup> ions in the ZSO electrolyte continuously migrate from bulk electrolytes to the interface and undergo a desolvation process prior to deposition. This introduces significant amounts of free water molecules during long-term cycling, triggering severe HER on the zinc surface [39]. Figure 2e illustrates the binding energies of Zn<sup>2+</sup>-H<sub>2</sub>O and Gd<sup>3+</sup>-H<sub>2</sub>O. Compared to Zn<sup>2+</sup> ions, Gd<sup>3+</sup> ions exhibit a stronger binding affinity to water molecules. Moreover, the binding energy between Gd<sup>3+</sup> ions

and water molecules decreases until the coordination number reaches nine (Figs. 2f and S3), indicating that the most stable solvation structure for  $Gd^{3+}$  ions is  $[Gd(H_2O)_9]^{3+}$ . This observation is consistent with the solvation number reported in prior work and suggests that  $Gd^{3+}$  ions can efficiently disrupt the HB networks among water molecules [40, 41]. In comparison, solvated  $Zn^{2+}$  ions typically coordinate with six water molecules in the ZSO electrolyte. The strong binding affinity and high coordinating capability of  $Gd^{3+}$  ions effectively suppress water-induced interfacial side reactions , thereby contributing to the stabilization of zinc anodes in sulfate electrolytes.

SEM images were obtained to investigate the morphology evolution of zinc deposits obtained in different electrolytes. In the ZSO electrolyte, zinc deposition initiates with uneven nucleation on the surface, which subsequently leads to the growth of large dendrites over time due to the tipping effect (Fig. S4). As depicted in Fig. 3a, these dendrites further develop into highly porous and moss-like clusters that can ultimately penetrate the glass fiber separator to induce battery short circuits. Notably, the formation of porous zinc deposits could be attributed to exacerbated detrimental side reactions (e.g., HER) occurring at the interface near dendrites [42]. In contrast, the zinc deposition layer obtained in the ZSO/Gd<sup>3+</sup> electrolyte remains smooth and free of notable protrusions (Figs. S4 and 3b) due to the microlevelling effect induced by Gd<sup>3+</sup> ions. The evenly deposited zinc ensures a homogenous distribution of electric field across the interface, thereby suppressing rampant dendrite growth and interfacial side reactions during subsequent deposition processes.

In situ optical microscopy was employed to investigate the dynamic zinc deposition behaviors in different electrolytes. Figure 3c displays optical images of the interface at different plating stages. In the ZSO electrolyte, uneven zinc deposits emerge on the surface after a plating duration of 5 min. By 25 min of plating, zinc deposits grow into large and irregular dendrites. Conversely, during zinc deposition in the ZSO/Gd<sup>3+</sup> electrolyte, the interface remains uniform and the thickness of the zinc deposition layer increases smoothly. To further quantify the morphological characteristics of zinc deposits, 3D-CLSM images were obtained. As shown in Fig. 3d, the zinc deposits obtained in the ZSO electrolyte exhibit a high surface roughness ( $R_a$ ) of 3.072 µm, attributed to randomly distributed dendrites. In contrast, the  $R_a$  of the zinc deposits obtained in the ZSO/Gd<sup>3+</sup> electrolyte significantly decreases to 0.781 µm (Fig. 3e), confirming that the microlevelling effect activated by Gd<sup>3+</sup> ions effectively suppresses dendrite growth.

To investigate the corrosion behavior, zinc foils immersed in the ZSO and ZSO/Gd<sup>3+</sup> electrolytes for 6 days were characterized using SEM. As depicted in Figs. 4a and S5, the zinc immersed in the ZSO electrolyte is covered by many



Fig. 3 Zinc deposition behaviors in different electrolytes. SEM images of the zinc deposited at 1 mA cm<sup>-2</sup> for 1 h in a ZSO and b ZSO/ $Gd^{3+}$  electrolytes. c In situ optical microscopy images of the zinc deposits obtained in different electrolytes. 3D-CLSM images of the zinc after cycling for 1 h in d ZSO and e ZSO/ $Gd^{3+}$  electrolytes

by-product platelets rich in O and S, with contents reaching 59.42% and 9.28%, respectively. This observation indicates that severe zinc corrosion occurs during immersion tests in the ZSO electrolyte. When the zinc foil is immersed in the ZSO/Gd<sup>3+</sup> electrolyte, the zinc surface shows no significant changes compared to its initial state (Figs. S6 and 4b). As shown in Fig. S7, only small amounts of O (5.41%) and S (0.02%) are present on the zinc surface, indicating a significant suppression of zinc corrosion in the ZSO/Gd<sup>3+</sup> electrolyte decreases to 1.59 (Fig. S8), no significant zinc corrosion occurs in this acidic electrolyte due to the preferential adsorption of Gd<sup>3+</sup> ions, consistent with the phenomenon reported in prior work [43]. The XRD results presented in Fig. 4c further

corroborate these findings. For the zinc immersed in the ZSO electrolyte, large amounts of  $Zn_4(SO_4)(OH)_6$ ·4H<sub>2</sub>O (ZHS) by-products are identified. Conversely, no by-product diffraction peaks are observed for the zinc immersed in the ZSO/Gd<sup>3+</sup> electrolyte.

Figure 4d, e schematically illustrates the difference between the ZSO and ZSO/Gd<sup>3+</sup> electrolytes. In conventional ZSO electrolytes, spontaneous zinc corrosion occurs at the water-rich interface and results in the formation of non-ion-conducting ZHS by-products (Fig. 4d). However, the zinc anode remains stable in the ZSO/Gd<sup>3+</sup> electrolyte due to the formation of a water-poor interface through the self-adsorption of Gd<sup>3+</sup> ions (Fig. 4e). This Gd<sup>3+</sup>-mediated water-poor interface effectively inhibits the occurring of



**Fig. 4** Zinc–electrolyte interface stability in different electrolytes. SEM and EDS images of the zinc surface immersed in **a** ZSO and **b** ZSO/ $Gd^{3+}$  electrolytes for 6 days. **c** XRD patterns of the zinc foil after immersion tests. Schematic illustrations of the EDL structures in **d** ZSO and **e** ZSO/ $Gd^{3+}$  electrolytes. **f** Tafel, **g** differential capacitance, **h** LSV and **i** CA curves of zinc electrodes tested in ZSO and ZSO/ $Gd^{3+}$  electrolytes

detrimental reactions (e.g., zinc corrosion, by-product formation). To further investigate zinc corrosion kinetics, Tafel tests were conducted in different electrolytes. As shown in Fig. 4f, the zinc electrode exhibits a corrosion current density of 0.154 mA cm<sup>-2</sup> in the ZSO/Gd<sup>3+</sup> electrolyte, which is lower than that (1.31 mA cm<sup>-2</sup>) of zinc obtained in the ZSO electrolyte. This indicates a substantial reduction in the zinc corrosion rate when Gd<sup>3+</sup> ions are present in the electrolyte, consistent with the findings obtained from immersion tests.

Figure 4g displays the differential capacitance-voltage curves of zinc electrodes in different solutions. The ZnSO<sub>4</sub> was substituted by  $Na_2SO_4$  in the solution to exclude the influence of Faradaic currents during testing. Compared with the Na<sub>2</sub>SO<sub>4</sub> solution, the zinc electrode exhibits a lower capacitance in the Gd<sup>3+</sup>-containing solution, which could be attributed to Gd<sup>3+</sup> adsorption and its large hydrated ionic radius [44]. Furthermore, as indicated in Fig. S9, the presence of Gd<sup>3+</sup> ions results in slightly reduced contact angles between the ZSO/Gd<sup>3+</sup> electrolyte and various electrodes (e.g., Cu, Zn, and NVO), suggesting improved interfacial wettability. The introduction of Gd<sup>3+</sup> ions also shifts the HER onset potential from -0.318 to -0.416 V at a current of 2 mA (Fig. 4h), demonstrating that the spontaneously formed Gd<sup>3+</sup> adsorption layer effectively suppresses HER kinetics. Additionally, as indicated by the CA curves (Fig. 4i), the current density of the zinc anode increases significantly under a constant overpotential in the ZSO electrolyte, indicating a pronounced tipping effect induced by 2D diffusion. In contrast, the introduction of Gd<sup>3+</sup> ions effectively transforms the  $Zn^{2+}$  diffusion mode to 3D, thus limiting the increase in current by suppressing zinc dendrite growth [45].

To investigate zinc plating kinetics, the activation energy  $(E_a)$  was calculated according to the Arrhenius equation [46]:

$$\frac{1}{R_{ct}} = A \exp\left(-\frac{E_a}{RT}\right) \tag{3}$$

where A is the Arrhenius constant,  $R_{ct}$  is the charge transfer resistance, R is the gas constant, and T is the temperature. Figures 5a and S10 present the EIS curves of the Zn//Zn symmetric cells based on ZSO/Gd<sup>3+</sup> and ZSO electrolytes at different temperatures, respectively. The  $E_a$  decreases from 20.72 kJ mol<sup>-1</sup> in the ZSO electrolyte to 18.91 kJ mol<sup>-1</sup> in the ZSO/Gd<sup>3+</sup> electrolyte (Fig. 5b), indicating that Gd<sup>3+</sup> ions effectively facilitate the desolvation of Zn<sup>2+</sup> ions upon zinc deposition. This reduction in desolvation energy barrier leads to a lower initial nucleation overpotential for zinc deposition in the ZSO/Gd<sup>3+</sup> electrolyte (Fig. S11). Figure 5c shows the CV curves for zinc plating/stripping. In both electrolytes, the redox peaks are located at similar positions and exhibit comparable shapes, validating the stability of Gd<sup>3+</sup> ions during zinc plating/stripping. In addition, Gd<sup>3+</sup> ions effectively decrease the onset overpotentials for zinc plating (Fig. S12), which implies improved reversibility and kinetics of zinc deposition in the ZSO/Gd<sup>3+</sup> electrolyte [47]. These improvements contribute to the superior rate capability of the Zn//Zn symmetric cell based on the ZSO/Gd<sup>3+</sup> electrolyte at current densities ranging from 0.5 to 10 mA cm<sup>-2</sup> (Fig. S13).

Figure 5d presents the cycling performance of Zn// Zn symmetric cells based on different electrolytes. At  $1 \text{ mA cm}^{-2}$  and  $1 \text{ mAh cm}^{-2}$ , the cycling life of Zn//Zn symmetric cells is dramatically extended from approximately 150 h with the ZSO electrolyte to over 2100 h with the ZSO/  $Gd^{3+}$  electrolyte. Even at 5 mA cm<sup>-2</sup> and 2 mAh cm<sup>-2</sup>, the Zn//Zn symmetric cell using the ZSO/Gd<sup>3+</sup> electrolyte maintains a long cycle life of 1000 h with stable voltage hysteresis (Fig. 5e). In comparison, the ZSO-based Zn//Zn symmetric cell experiences dendrite-induced short circuits after 240 h. Figure 5f shows the surface morphologies of the cycled zinc anode in symmetric cells. In the ZSO electrolyte, the zinc anode exhibits a rough and highly dendritic morphology due to uneven zinc deposition. Meanwhile, the surface of the zinc anode remains smooth and free of by-product flakes when cycled in the ZSO/Gd<sup>3+</sup> electrolyte, indicating the effective suppression of ZHS and Gd<sup>3+</sup>-containing by-products (e.g., gadolinium hydroxide and gadolinium hydroxide sulfate) that typically possess a layered structure [48, 49]. As further confirmed by the XPS spectra presented in Fig. S14, only trace amounts of  $Gd^{3+}$  and  $SO_4^{2-}$  ions are precipitated onto the zinc surface during cycling, which is distinct from the fast and severe passivation of ZHS in conventional zinc sulfate electrolytes [49, 50]. Figure 5g schematically illustrates the significant inhibition effect of Gd<sup>3+</sup> ions on dendrite growth. In the ZSO electrolyte, Zn<sup>2+</sup> ions are accumulated at surface protrusions due to the tipping effect, resulting in preferential deposition of Zn<sup>2+</sup> ions at these tips. However, in the ZSO/Gd<sup>3+</sup> electrolyte, the protruding locations are occupied by Gd<sup>3+</sup> ions, which have stronger electrostatic attraction with the negatively charged zinc surface. This creates an electrostatic shielding layer that effectively repels  $Zn^{2+}$  ions, preventing them from acquiring



**Fig. 5** Electrochemical reversibility and stability of zinc metal anodes. **a** EIS curves of the Zn//Zn symmetric cells with the ZSO/Gd<sup>3+</sup> electrolyte at different temperatures. **b** Activation energies of  $Zn^{2+}$  desolvation in different electrolytes. **c** CV curves of Zn//Cu batteries with ZSO and ZSO/Gd<sup>3+</sup> electrolytes. Cycling performance of Zn//Zn symmetric cells at **d** 1 mA cm<sup>-2</sup>, 1 mAh cm<sup>-2</sup> and **e** 5 mA cm<sup>-2</sup>, 2 mAh cm<sup>-2</sup>. **f** SEM images of the zinc anodes cycled in Zn//Zn symmetric cells. **g** Schematic illustrations of the zinc deposition behaviors in different electrolytes

electrons at protrusions. Consequently,  $Zn^{2+}$  ions preferentially deposit in regions surrounding the protrusions, activating the microlevelling effect and thus promoting uniform zinc deposition.

To evaluate the zinc plating/stripping reversibility, Zn//Cu asymmetric cells were assembled and tested. At 2 mA cm<sup>-2</sup> and 1 mAh cm<sup>-2</sup>, the cycle life of the Zn//Cu asymmetric cells is significantly extended from less than 200 cycles with the ZSO electrolyte to over 1400 cycles with the ZSO/ $Gd^{3+}$  electrolyte (Fig. 6a). In addition, the ZSO-based Zn//Cu cell shows an average CE of only 98.44%, which is noticeably lower than the 99.72% achieved by the Zn//Cu cell with the ZSO/ $Gd^{3+}$  electrolyte. As shown in Fig. 6b, c, the poor zinc plating/stripping reversibility in the ZSO

electrolyte results in a significant higher voltage hysteresis for the Zn//Cu cell compared to that of the ZSO/Gd<sup>3+</sup> electrolyte. Such improvement in zinc plating/stripping could be mainly attributed to Gd<sup>3+</sup> ions, which enable the formation of a water-poor EDL, thereby suppressing side reactions (e.g., HER, by-product formation). Similar improvements are observed for the Zn//Cu cells cycled at 1 mA cm<sup>-2</sup> (Fig. S15), further confirming the effectiveness of Gd<sup>3+</sup> ions in promoting zinc plating/stripping reversibility under different conditions.

To comprehensively investigate the performance of the ZSO/Gd<sup>3+</sup> electrolyte in practical applications, NVO cathode material was synthesized following our previously reported method [50, 51]. The SEM image and XRD pattern shown in

Fig. S16 confirm the successful synthesis of NVO powders. As shown in Fig. 6d, the Zn//NVO full cell with the ZSO electrolyte exhibits an interfacial impedance of 166  $\Omega$ , which is comparable to the value reported in prior work [51, 52]. When utilizing the  $ZSO/Gd^{3+}$  electrolyte, the interfacial impedance of the Zn//NVO full cell significantly decreases to  $88.6 \Omega$  due to enhanced charge transfer kinetics. Figure 6e presents the CV curves of the full cells at 0.1 mV s<sup>-1</sup> within a voltage window of 0.4-1.4 V. No additional oxidation/reduction peaks are observed in the presence of Gd<sup>3+</sup> ions, confirming their inert nature and long-term effectiveness in regulating zinc deposition. Furthermore, the full cell utilizing the ZSO/Gd<sup>3+</sup> electrolyte displays higher redox peak currents compared to the ZSO-based full cell. This observation indicates that Gd<sup>3+</sup> ions effectively improve zinc intercalation/deintercalation kinetics for the NVO cathode.

Figure 6f presents the cycling stability of Zn//NVO full cells at 5 A g<sup>-1</sup>. The ZSO-based Zn//NVO full cell exhibits fast capacity degradation due to poor zinc plating/stripping reversibility. In comparison, the Zn//NVO full cell with the ZSO/ Gd<sup>3+</sup> electrolyte demonstrates remarkably enhanced cycling stability with a high capacity retention rate of 85.6% after 1000 cycles, outperforming most previously reported AZIBs based on electrolytes containing other metallic cations (Table S1). Consistently, the ZSO/Gd<sup>3+</sup> electrolyte effectively improves the cycling stability of the Zn//NVO full cell at 2 A  $g^{-1}$  (Fig. S17). As shown in Fig. 6g, the zinc anode cycled in the ZSObased full cell displays a mossy and dendritic surface due to uneven zinc deposition and side reactions, leading to rapid capacity decay. However, upon introducing  $Gd^{3+}$  ions, the zinc anode in the full cell after cycling remains free of dendrites and by-products (Fig. 6h). Therefore, the long-term stability



**Fig. 6** Electrochemical performance of ZSO/Gd<sup>3+</sup> electrolyte. **a** CE of zinc plating/stripping in Zn//Cu batteries at 2 mA cm<sup>-2</sup> and 1 mAh cm<sup>-2</sup>. Voltage–capacity curves of Zn//Cu batteries with **b** ZSO and **c** ZSO/Gd<sup>3+</sup> electrolytes. **d** EIS and **e** CV curves of Zn//NVO full cells. **f** Cycling performance of Zn//NVO full cells at 5 A g<sup>-1</sup>. SEM images of the zinc anodes obtained in full cells with **g** ZSO and **h** ZSO/Gd<sup>3+</sup> electrolytes after 1000 cycles at 5 A g<sup>-1</sup>. **i** Rate performance of Zn//NVO full cells at different current densities

**Conflict of Interest** The authors declare no interest conflict. They have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper. Prof. Jiang Zhou is an editorial board member for Nano–Micro Letters and was not involved in the editorial review or the decision to publish this article.

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of the full cell based on the ZSO/Gd<sup>3+</sup> electrolyte is effectively improved. Additionally, the ZSO/Gd<sup>3+</sup> electrolyte enhances rate performance of the Zn//NVO full cells. As illustrated in Figs. 6i and S18, the specific capacities of the full cell with the ZSO/Gd<sup>3+</sup> electrolyte are significantly higher than those of the ZSO-based full cell at current densities ranging from 0.5 to 10 A g<sup>-1</sup>, further affirming the positive impact of Gd<sup>3+</sup> ions on the electrochemical performance of AZIBs.

## **4** Conclusions

In conclusion, Gd<sup>3+</sup> ions are introduced into conventional zinc sulfate electrolytes as a microlevelling agent to enable highly reversible and stable zinc anodes. The adsorbed Gd<sup>3+</sup> ions not only inhibit the tipping effect at protrusions but also form a water-poor EDL near the zinc surface by substituting interfacial water molecules. Electrochemical tests and materials characterization collaboratively confirm that the adsorption of  $Gd^{3+}$  ions is beneficial in inhibiting interfacial side reactions and suppress zinc dendrite growth. Consequently, the Zn//Zn symmetric cell with the ZSO/Gd<sup>3+</sup> electrolyte exhibits remarkably improved cycling stability for over 2100 h at a 1 mA cm<sup>-2</sup> and 1 mAh cm<sup>-2</sup>. Meanwhile, when paired with the ZSO/Gd<sup>3+</sup> electrolyte, the Zn//Cu asymmetric cell achieves a high average CE of 99.72% over 1400 cycles and the Zn//NVO full cell demonstrates a high capacity retention rate of 85.6% after 1000 cycles at 5 A  $g^{-1}$ . This work provides novel perspectives and insights for the development of highly efficient and durable AZIBs.

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